

## **AMENDMENTS TO THE CLAIMS**

This listing of claims will replace all prior versions, and listings, of claims in the application.

### **Listing of Claims:**

- Claim 1      (Previously Presented) A process for oligomerizing the olefins present in a Fischer-Tropsch derived condensate containing a mixture of olefins and oxygenates which comprises:
- (a) removing substantially all of the oxygenates present in the Fischer-Tropsch condensate using a molecular sieve adsorbent having a low silica to alumina ratio, said molecular sieve being effective for removing oxygenates;
  - (b) contacting the Fischer-Tropsch derived condensate containing substantially no oxygenates with an ionic liquid catalyst in an oligomerization zone under oligomerization reaction conditions; and
  - (c) recovering from the oligomerization zone a Fischer-Tropsch derived product having molecules characterized by a higher average molecular weight and increased branching as compared to the Fischer-Tropsch derived condensate.
- Claim 2, 3 and 4 (Cancelled)
- Claims 5 and 6      (Cancelled)
- Claim 7      (Previously Presented) The process of claim 1 wherein the molecular sieve is a large pore zeolite.

- Claim 8 (Previously Presented) The process of claim 1 wherein the molecular sieve has an FAU type framework.
- Claim 9 (Original) The process of claim 7 wherein the molecular sieve is an X zeolite.
- Claim 10 (Original) The process of claim 7 wherein the molecular sieve is a 13X molecular sieve.
- Claim 11 (Previously Presented) A process for preparing a Fischer-Tropsch derived product by the oligomerization of the olefins in a Fischer-Tropsch derived concentrate which contains olefins and oxygenates which comprises:
- (a) dehydrating the Fischer-Tropsch derived concentrate in a dehydration zone under dehydration conditions and recovering a dehydrated Fischer-Tropsch derived condensate from the dehydration zone;
  - (b) contacting the dehydrated Fischer-Tropsch derived condensate with a molecular sieve capable of adsorbing substantially all of the oxygenates remaining in the dehydrated Fischer-Tropsch derived condensate and recovering a Fischer-Tropsch derived condensate intermediate containing substantially no oxygenates;
  - (c) contacting the Fischer-Tropsch derived condensate intermediate in an oligomerization zone with an effective oligomerizing amount of a Lewis acid ionic liquid oligomerization catalyst while maintaining said Fischer-Tropsch derived condensate intermediate and said oligomerization catalyst under preselected oligomerization

conditions for a sufficient time to oligomerize the olefins present; and

- (d) recovering from the oligomerization zone a Fischer-Tropsch derived product having molecules characterized by a higher average molecular weight and increased branching as compared to the Fischer-Tropsch derived condensate.

Claim 12 (Cancelled)

Claim 13 (Cancelled)

Claim 14 (Cancelled)

Claim 15 (Original) The process of claim 11 wherein the adsorbent of step (b) is a molecular sieve having low silica to alumina ratio.

Claim 16 (Original) The process of claim 15 wherein the molecular sieve of step (b) has an FAU type framework.

Claim 17 (Original) The process of claim 16 wherein the molecular sieve is an X zeolite.

Claim 18 (Original) The process of claim 16 wherein the molecular sieve of step (b) is a 13X molecular sieve.

Claim 19 (Original) The process of claim 11 wherein the Lewis acid ionic oligomerization catalyst comprises a first component and a second component, said first component comprising a compound selected from the group consisting of aluminum halide, alkyl aluminum halide, gallium halide, and alkyl gallium halide, and said second component is quaternary ammonium or quaternary phosphonium salt.

- Claim 20 (Original) The process of claim 19 wherein said first component is aluminum halide or alkyl aluminum halide.
- Claim 21 (Original) The process of claim 20 wherein said first component is aluminum trichloride.
- Claim 22 (Original) The process of claim 19 wherein said second component is selected from one or more of hydrocarbyl substituted ammonium halide, hydrocarbyl substituted imidazolium halide, hydrocarbyl substituted pyridinium halide, alkylene substituted pyridinium dihalide, or hydrocarbyl substituted phosphonium halide.
- Claim 23 (Original) The process of claim 22 wherein the second component is an alkyl substituted quaternary ammonium halide containing one or more alkyl moieties having from 1 to about 9 carbon atoms.
- Claim 24 (Original) The process of claim 23 wherein the second component comprises at least trimethylamine hydrochloride.
- Claim 25 (Original) The process of claim 22 wherein the second component is an alkyl substituted imidazolium halide.
- Claim 26 (Original) The process of claim 25 wherein the second component comprises at least 1-ethyl-3-methyl-imidazolium chloride.
- Claim 27 (Original) The process of claim 22 wherein the ratio of first component to the second component of the oligomerization catalyst is within the range of from about 1:1 to about 5:1.

- Claim 28 (Original) The process of claim 19 wherein the ratio of the first component to the second component is within the range of from about 1:1 to about 2:1.
- Claim 29 (Previously Presented) The process of claim 11 including the additional step of hydrogenating the unsaturated double bonds present in the Fischer-Tropsch derived product.
- Claim 30 (Original) The process of claim 29 wherein the Fischer-Tropsch derived product includes lubricating base oil.
- Claim 31 (Original) The process of claim 29 wherein the Fischer-Tropsch derived product includes a diesel product.